

# MULTI-FIDELITY UNCERTAINTY QUANTIFICATION FOR GAS-SOLID FLOWS

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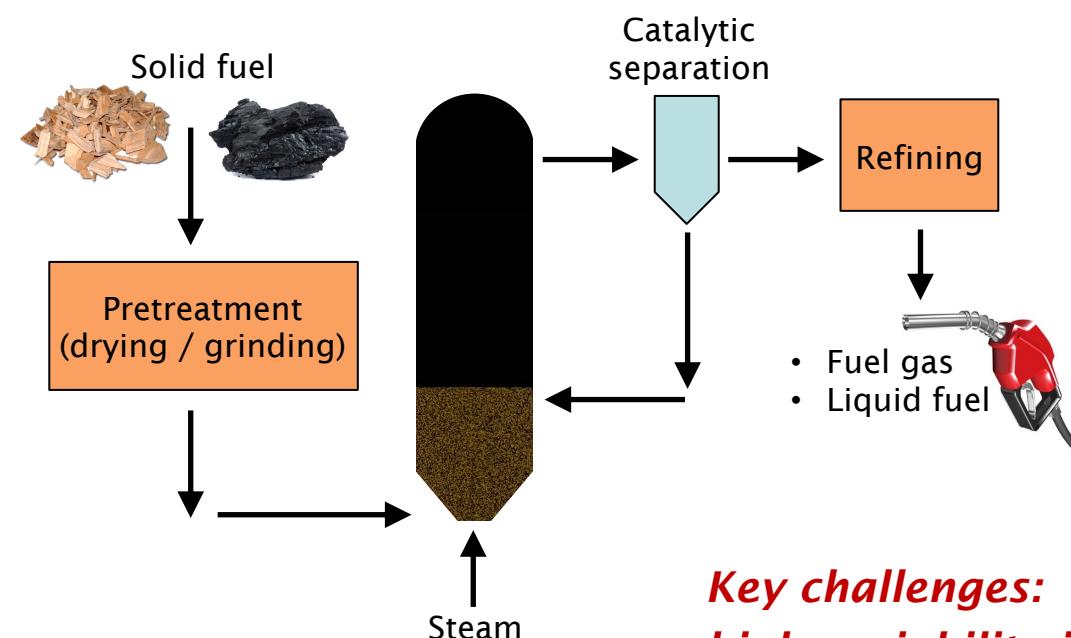
*2021 NETL Workshop on Multiphase Flow Science  
Tuesday, Aug 03, 2021*



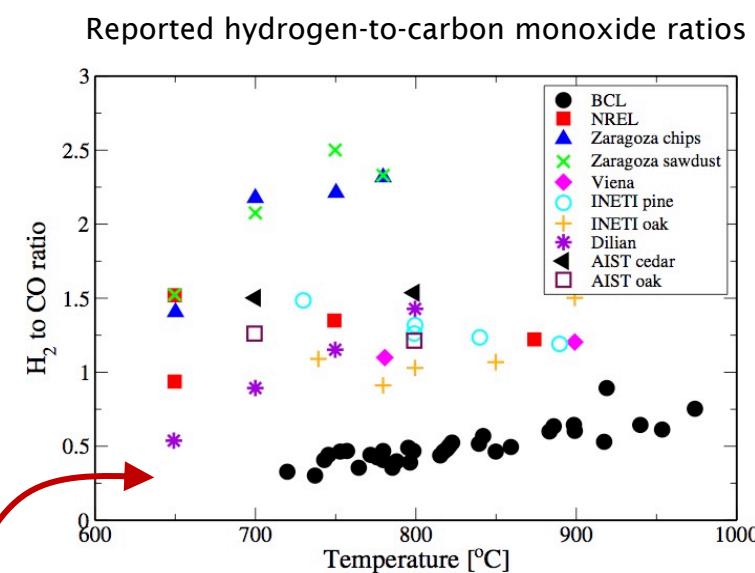
# Gas-solid flows are key to many chemical processes

*Fluidized bed reactors are at the heart of nearly all chemical transformation processes*

- Conventional technologies: Catalytic-like processes (*e.g.*, FCC) remain the primary conversion technique within petrochemical industry
- Emerging technologies: biomass pyrolysis, zero-carbon coal combustion

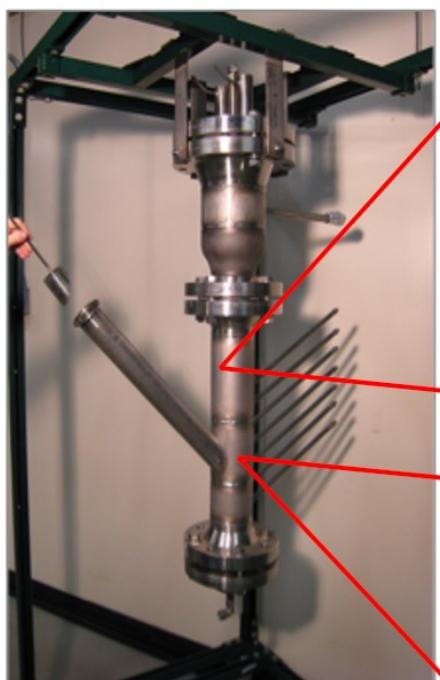


*Key challenges:  
high variability in reactor performance*

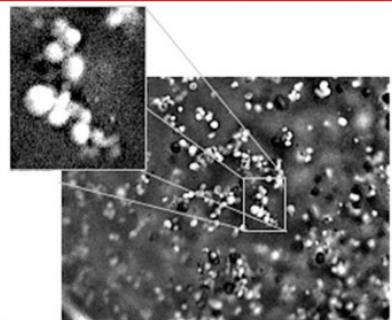


# Wall deposition contributes to reactor performance variations

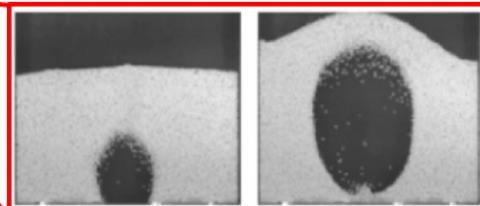
Cohesion and deposition of Geldart-A/C particles significantly impact the reactor performance



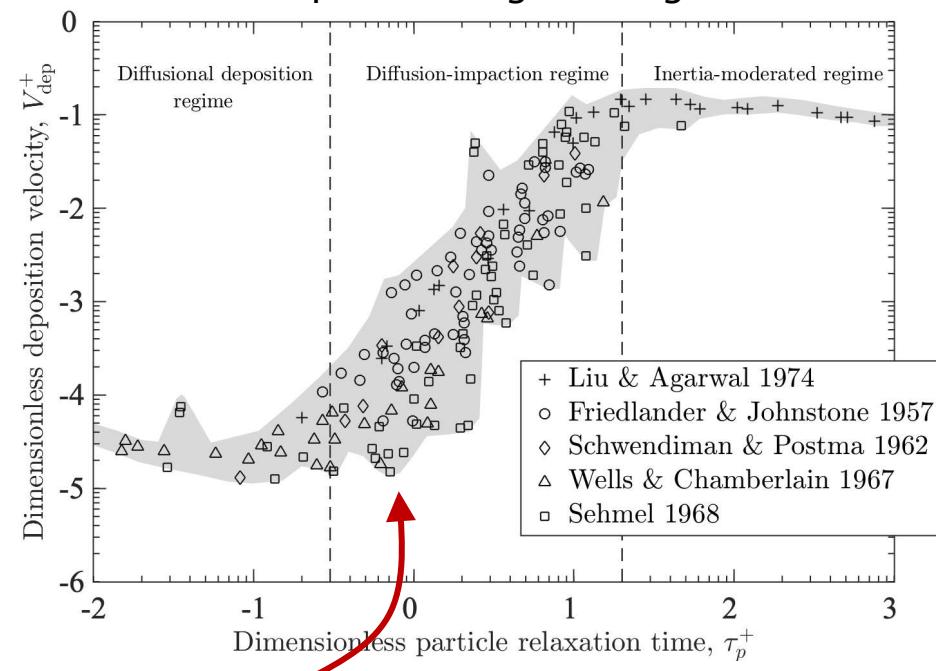
Wall cohesion



Bubbling



Deposition regime diagram



**Large uncertainties observed from experimental measurements**

# *Large underlying uncertainties in particle material properties*

*The physical properties of Geldart-A/C (e.g., catalyst, dust) particles can vary by orders of magnitude, which pose further modeling challenges*

Particle types	$d_p$ [ $\mu\text{m}$ ]	Hamaker constant [1e-20 J]		Electric charge [C]	CoR
		$A_{11}$	$A_{12}$		
$\text{SiO}_2$ (Silica)	0.1 – 100	6.5	5.37 – 13.7	8.0e-18 – 4.0e-16	0.62 – 0.77
$\text{SiO}_2$ (Quartz)	0.5 – 15	8.86	7.59 – 12.1	8.0e-18 – 4.0e-16	0.19
$\text{Al}_2\text{O}_3$ (Alumina)	0.2 – 34	15.2	7.90 – 21.1	1.4e-18 – 2.4e-16	0.62
$\text{CaSO}_4$ (Gypsum)	0.7 – 20	–	–	–	0.10
Dolomite	2 – 40	7.34 – 13.75	–	–	0.15
$\text{NaCl}$ (Salt)	–	6.48	6.45 – 10.3	–	0.11
$\text{Fe}_2\text{O}_3$	–	6.8 – 25	–	–	–
$\text{MgO}$	–	10.6 – 12.1	8.84 – 14.2	–	–
$\text{CaO}$	–	12.4	–	–	–
$\text{TiO}_2$	–	15.3	9.46 – 15.4	–	–
ARD	1 – 40	1.76 – 125	N/A	1.08e-17 – 5.2e-16	0.34 – 0.76
Fly ash	1.5 – 80	0.25 – 1.9	N/A	8.7e-17 – 2.2e-16	0.16 – 0.75
Fine soil	2 – 20	1.05 – 513	N/A	2.3e-17 – 2.5e-16	0.38 – 0.92

# *Large underlying uncertainties in particle material properties*

*The physical properties of Geldart-A/C (e.g., catalyst, dust) particles can vary by orders of magnitude, which pose further modeling challenges*

## **Main objectives:**

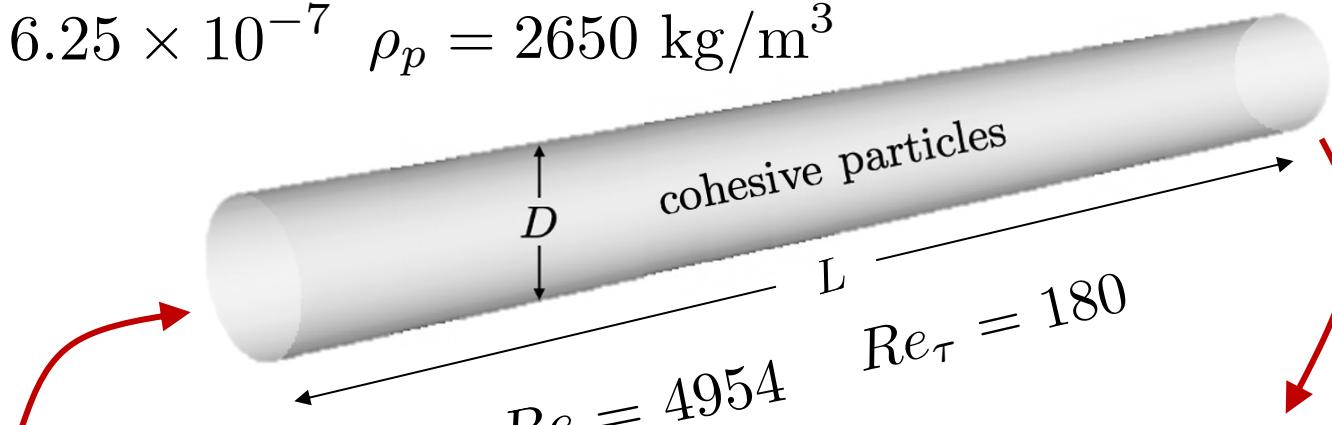
1. Develop particle deposition models of different fidelity to predict deposition rate in the presence of cohesion
2. Quantify the uncertainties and sensitivities of deposition on cohesion strength efficiently by leveraging these models
3. Understand the role of temperature on deposition rates

Fly ash	1.5 – 80	0.25 – 1.9	N/A	8.7e-17 – 2.2e-16	0.16 – 0.75
Fine soil	2 – 20	1.05 – 513	N/A	2.3e-17 – 2.5e-16	0.38 – 0.92

# A unit test case for particle deposition UQ and sensitivity analysis

$$D = 20 \text{ mm} \quad L = 10D \quad U_b = 4.0 \text{ m/s}$$

$$\varepsilon_p = 6.25 \times 10^{-7} \quad \rho_p = 2650 \text{ kg/m}^3$$



## **Input parameters:**

$$\xi = q_p/q_{\max} \in [0, 0.1]$$

$$q_{\max} = 500 \times (1.6 \times 10^{-19}) (d_p/10^{-6})^2$$

$$\zeta = A/A_0 \in [0, 1]$$

$$A_0 = 1.0 \times 10^{-18}$$

## **QoI:**

$$V_{\text{dep}}^+ \equiv \frac{V_{\text{dep}}}{u_*} = \frac{J_w}{\rho_{pm} u_*}$$

## **Statistics:**

- Mean
- Variance
- Sobol index

# High-fidelity model – DNS-DEM framework

- NGA<sup>1</sup>
  - Finite volume DNS code
  - Massively parallel
  - Conservation of mass, momentum, and kinetic energy

- Lagrangian particle tracking<sup>2</sup>

*Need to compute efficiently!*  
 [Yao & Capecelatro (2018) PRF]<sup>3</sup>  
 [Yao & Capecelatro (2021) JFM]<sup>4</sup>

– Position:  $\frac{d\mathbf{x}_p^{(i)}}{dt} = \mathbf{v}_p^{(i)}$

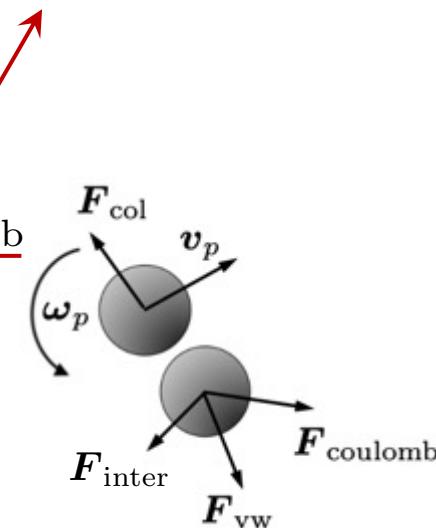
Collisions: Soft-sphere  
(mass-spring-damper)

– Velocity:  $m_p \frac{d\mathbf{v}_p^{(i)}}{dt} = \underline{\mathbf{F}_{\text{drag}}^{(i)}} + \underline{\mathbf{F}_{\text{col}}^{(i)}} + \underline{\mathbf{F}_{\text{vw}}^{(i)}} + \underline{\mathbf{F}_{\text{coulomb}}^{(i)}}$

– Angular velocity: Drag: Tenneti et al. (2011)

$$I_p \frac{d\boldsymbol{\omega}_p^{(i)}}{dt} = \sum_j \frac{d_p}{2} \mathbf{n}_{ij} \times \underline{\mathbf{f}_{t,j \rightarrow i}^{\text{col}}}$$

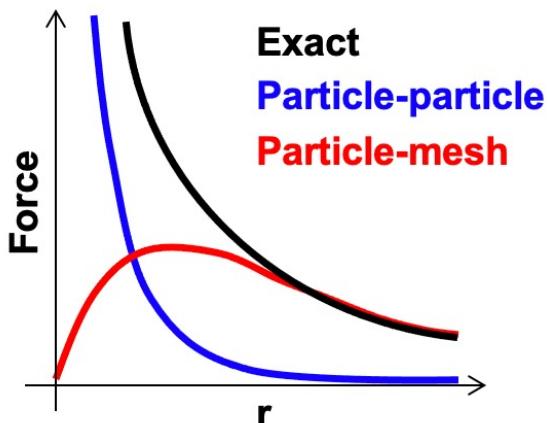
Collisions: Coulomb friction



1. O. Desjardins et al. (2008), JCP.
2. J. Capecelatro and O. Desjardins. (2013), JCP, 238:1–31.
3. Y. Yao and J. Capecelatro. (2018), PRF, 3(3):034301.
4. Y. Yao and J. Capecelatro. (2021), JFM, 911, A10.

# A brief note on the electrostatics and van der Waals algorithms

## An accurate electrostatic algorithm – P3M:

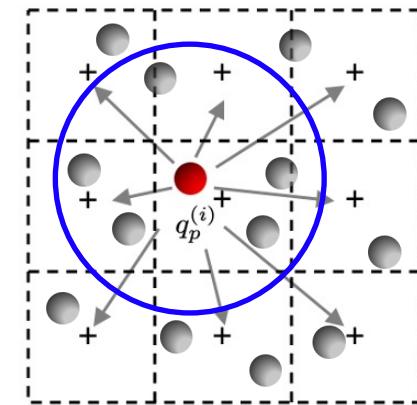


*Efficient using FFT*

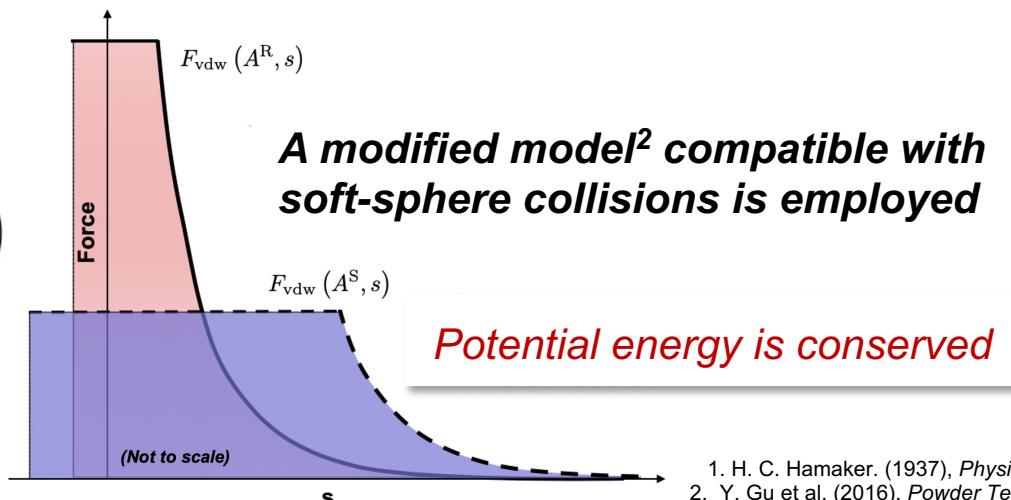
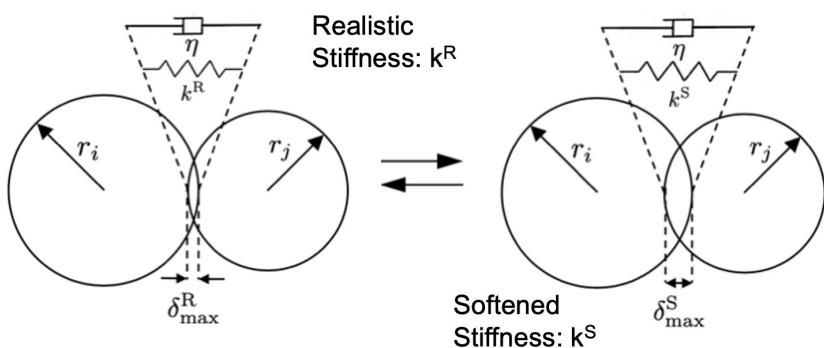
Long range:  $E_l(\mathbf{x}, t) = -\nabla \phi(\mathbf{x}, t)$   $k^2 \hat{\phi}_l(\mathbf{k}) = \frac{\hat{\rho}_l(\mathbf{k})}{\epsilon_0}$

Short range: if  $r_{ij} < r_{\max}$   $F_s(r_{ij}) = q_i q_j / (4\pi\epsilon_0 r_{ij}^2) - F_d(r_{ij})$

*Double counting removed*



**Van der Waals (Hamaker 1937)<sup>1</sup>:**  $F_{vdw}(A, s) = \frac{A}{3} \frac{2r_i r_j (r_i + r_j + s)}{s^2 (2r_i + 2r_j + s)^2} \left[ \frac{s(2r_i + 2r_j + s)}{(r_i + r_j + s)^2 - (r_i - r_j)^2} - 1 \right]^2$

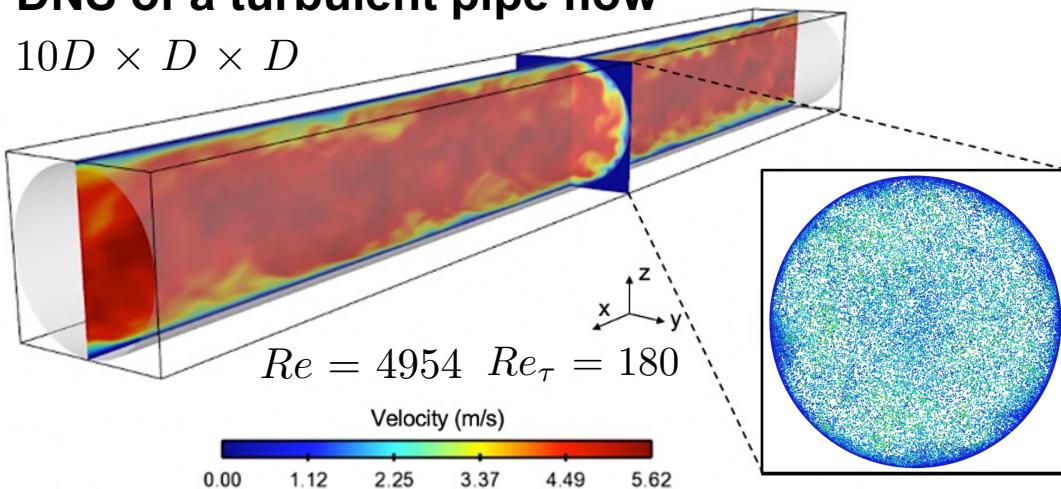


1. H. C. Hamaker. (1937), *Physica*.
2. Y. Gu et al. (2016), *Powder Tech.*

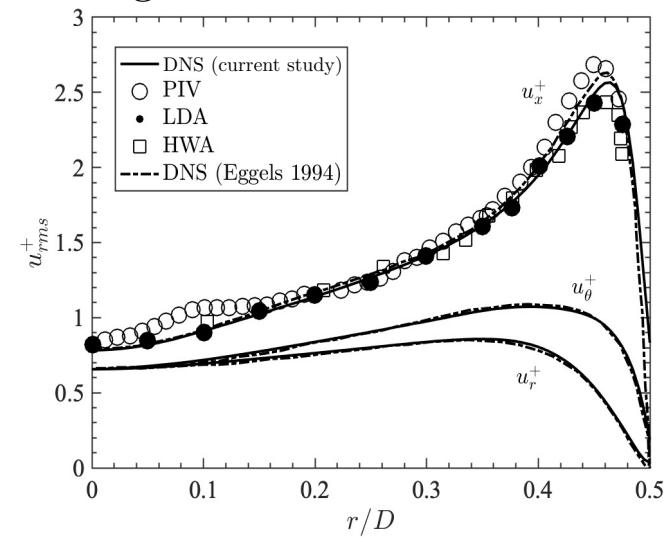
# High-fidelity model – DNS-DEM framework

## DNS of a turbulent pipe flow

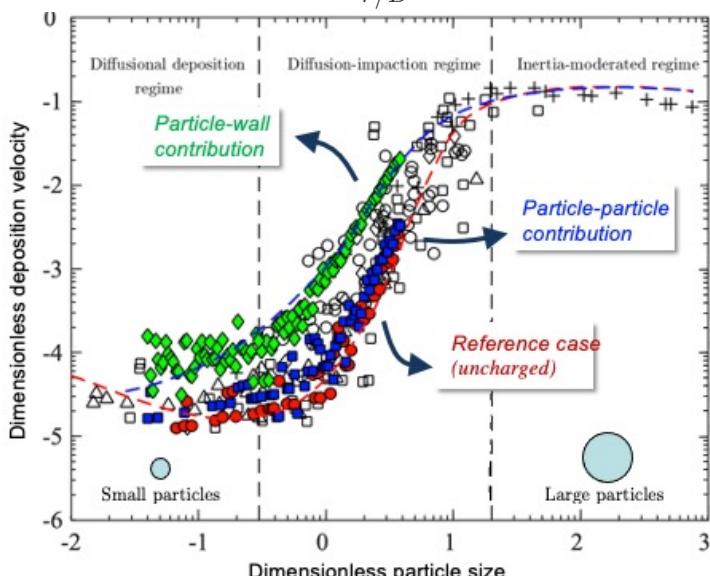
$10D \times D \times D$



grid =  $326 \times 256 \times 256$



- Non-dimensional deposition rate:
$$V_{\text{dep}}^+ = \left( \frac{\Delta N_{\text{dep}} D}{4\Delta t (N_0 - \Delta N_{\text{dep}})} \right) / u_*$$
- Particles counted as deposited once they hit the wall (all-stick assumption)
- 256 CPU hours required for converged statistics for each set of inputs ( $\zeta, \xi$ )

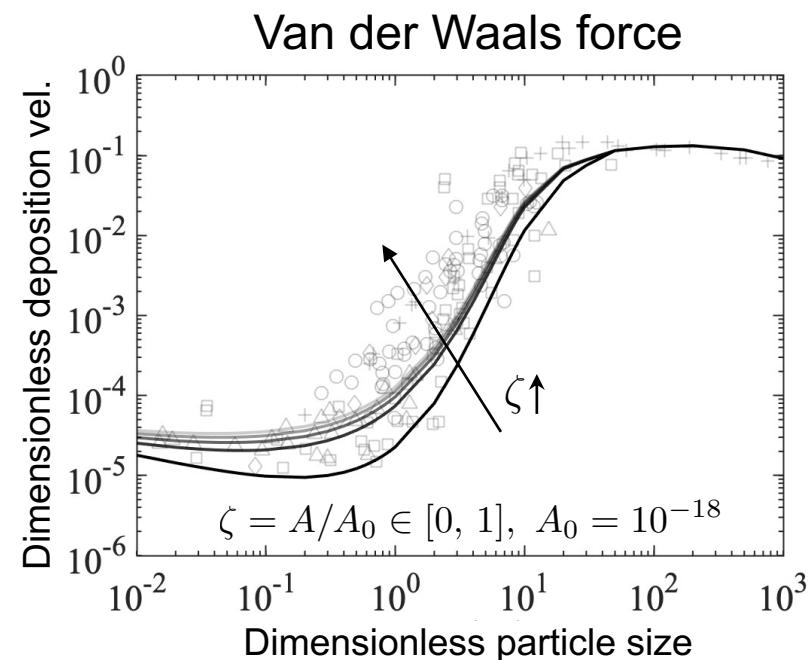
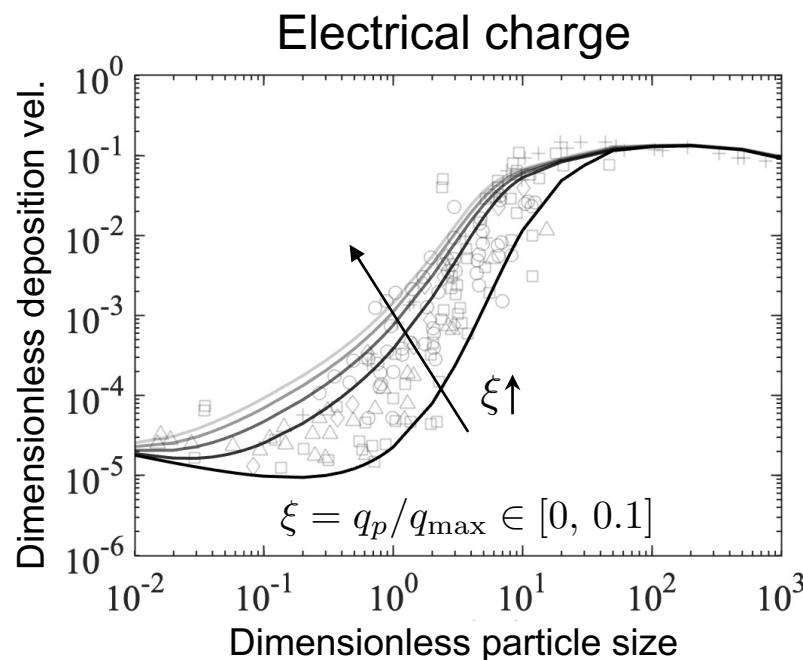


# Low-fidelity model – 1D Eulerian conservation equations

- A 1D Eulerian-based model by Guha<sup>1</sup> predicts deposition reasonably well, which is leveraged here to provide ‘low-fidelity’ predictions.

**Momentum:**  $\bar{V}_{py}^+ \frac{\partial \bar{V}_{py}^+}{\partial y^+} + \frac{\bar{V}_{py}^+}{\tau_p^+} = -\frac{\partial}{\partial y^+} \left( \Re \bar{V}_{fy}^{'+2} \right) + F_{\text{elec}}^+ + F_{\text{vdw}}^+$

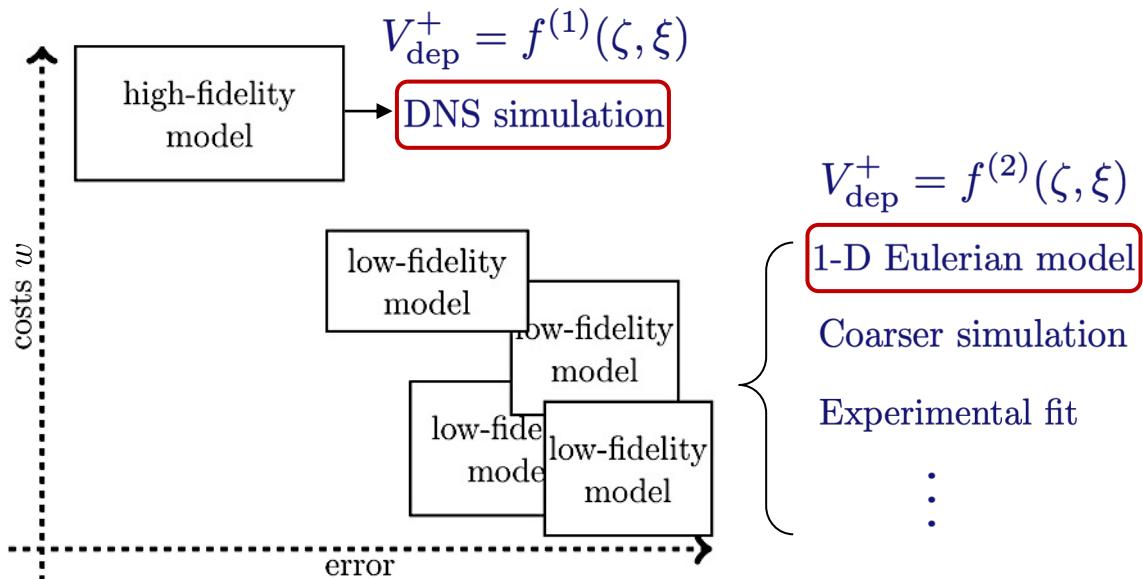
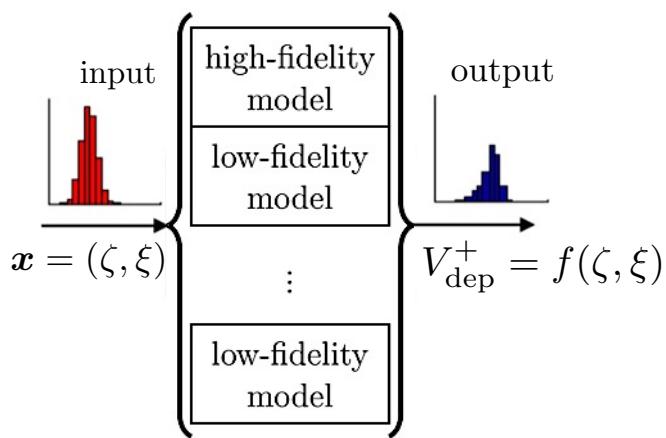
**Mass:**  $\partial V_{\text{dep}}^+ / \partial y^+ = 0, \quad V_{\text{dep}}^+ = - \left( \frac{D_B}{\nu} + \frac{\varepsilon}{\nu} \right) \frac{\partial \rho_p^+}{\partial y^+} + \rho_p^+ \bar{V}_{py}^+$



1. A. Guha. (2008), *Annu. Rev. Fluid Mech.*

# Multi-fidelity uncertainty quantification<sup>1</sup>

- **Goal: quantify how deposition rate depends on uncertainties in charge and van der Waals efficiently**



- Classic Monte Carlo (MC) estimator:  $\bar{y}_{m_1} = \frac{1}{m_1} \sum_{j=1}^{m_1} f^{(1)}(\mathbf{x}_j)$ ,  $\bar{y}_{m_2} = \frac{1}{m_2} \sum_{j=1}^{m_2} f^{(2)}(\mathbf{x}_j)$
- Multi-fidelity Monte Carlo (MFMC) estimator:  $\hat{s} = \bar{y}_{m_1} + \alpha_2 \left( \bar{y}_{m_2}^{(2)} - \bar{y}_{m_1}^{(2)} \right)$

*Find the optimal  $m_1$ ,  $m_2$ ,  $\alpha_2$  to minimize estimator error under the constraint:  $m_1 w_1 + m_2 w_2 \leq p$*

# 1D Eulerian model underpredicts deposition compared to DNS

## Prior estimates of model statistics:

- DNS: ~256 CPU hours  
 $w_1 = 1$
- 1D model: ~0.08 CPU hour  
 $w_2 = 1/2880$
- Correlation coefficients:  
 $\rho_{1,2} = \frac{\text{Cov}[f^{(1)}(X), f^{(2)}(X)]}{\sigma_1 \sigma_2}$

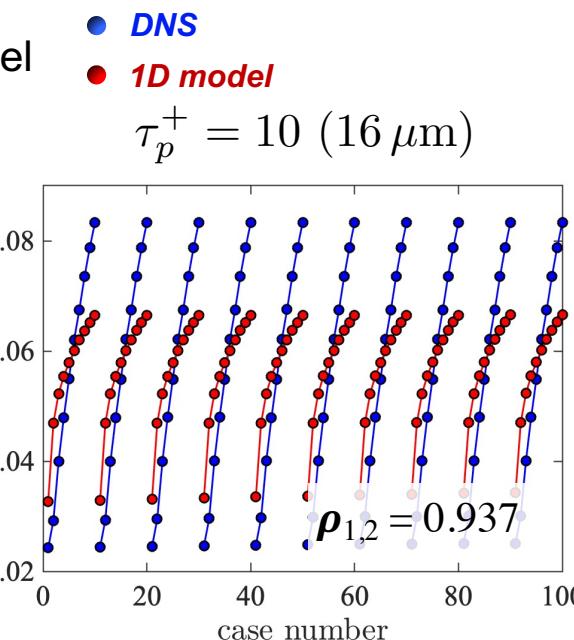
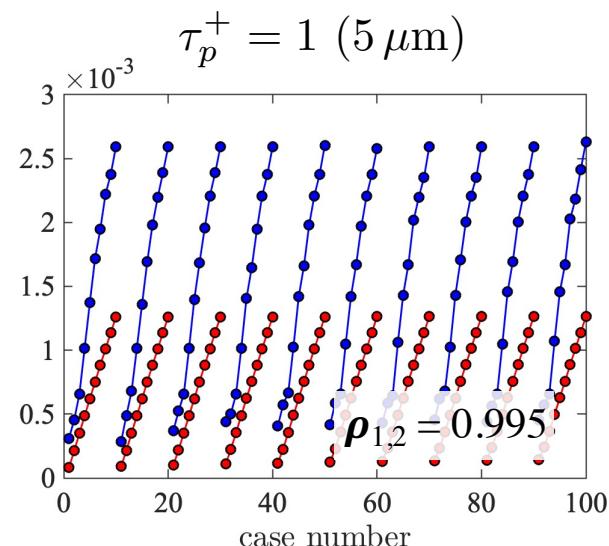
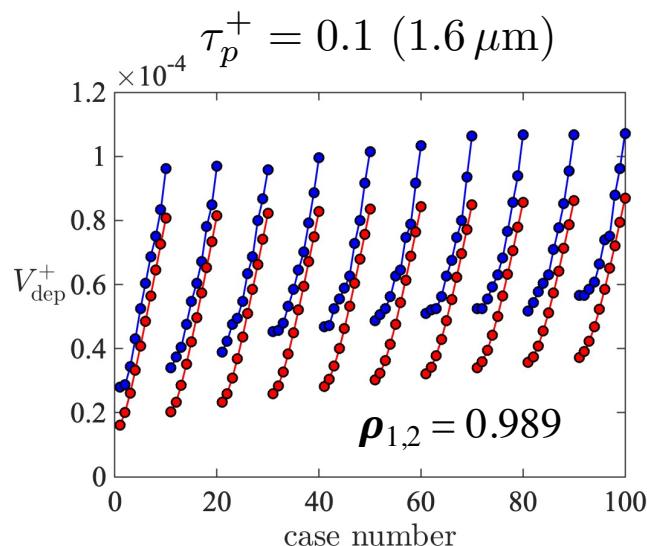


An analytical solution exists for the MFMC optimization<sup>1</sup>!

$$(\alpha_2, m_1, m_2) = \text{MFMC}(\rho_{1,2}, w_1, w_2, \sigma_1, \sigma_2)$$

$$\hat{s}_{\text{MFMC}} = \hat{s}_{\text{MC},m_1} + \alpha_2 \left( \hat{s}_{\text{MC},m_2}^{(2)} - \hat{s}_{\text{MC},m_1}^{(2)} \right)$$

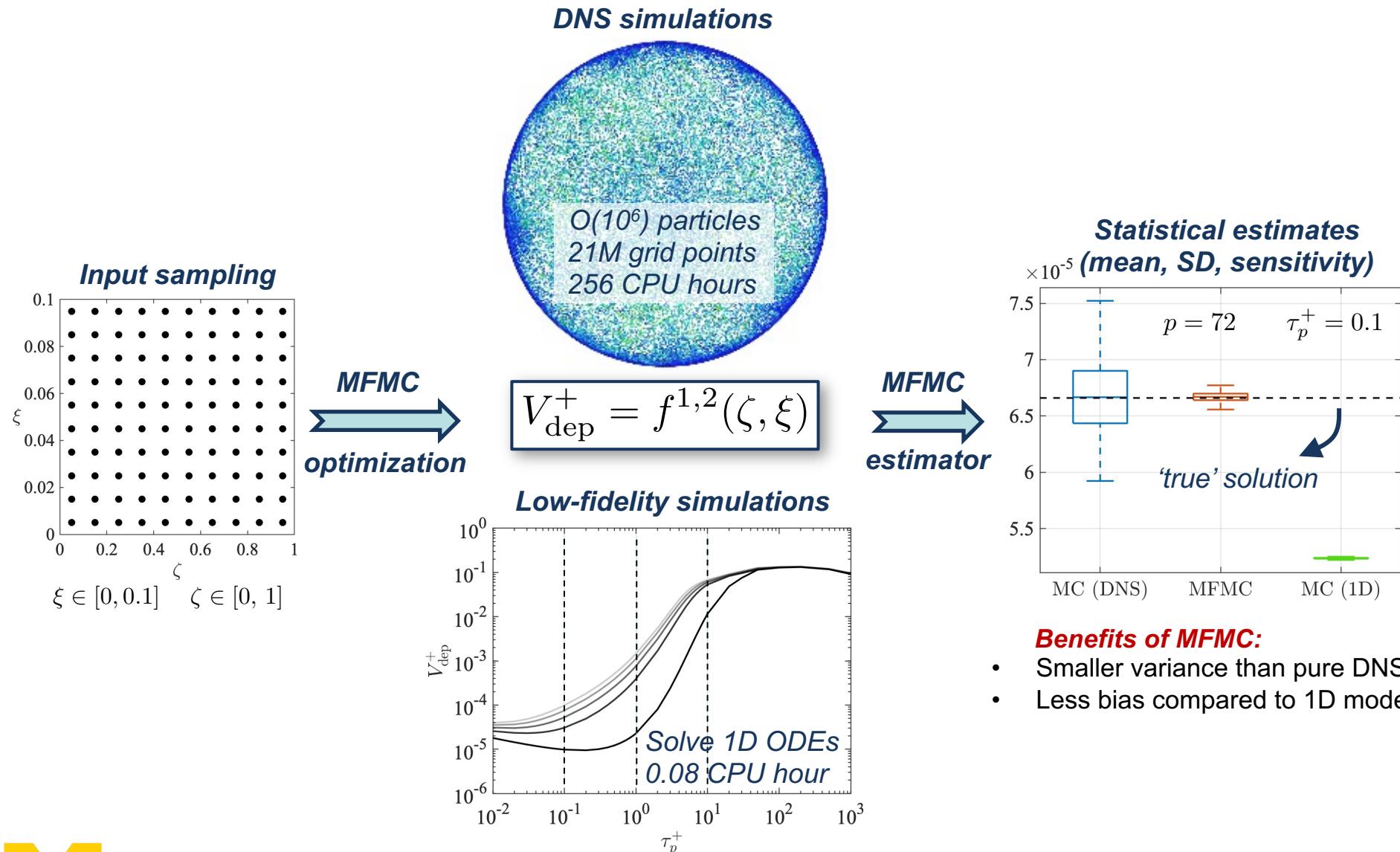
- Comparison of deposition predictions from DNS and 1D model



- DNS
- 1D model

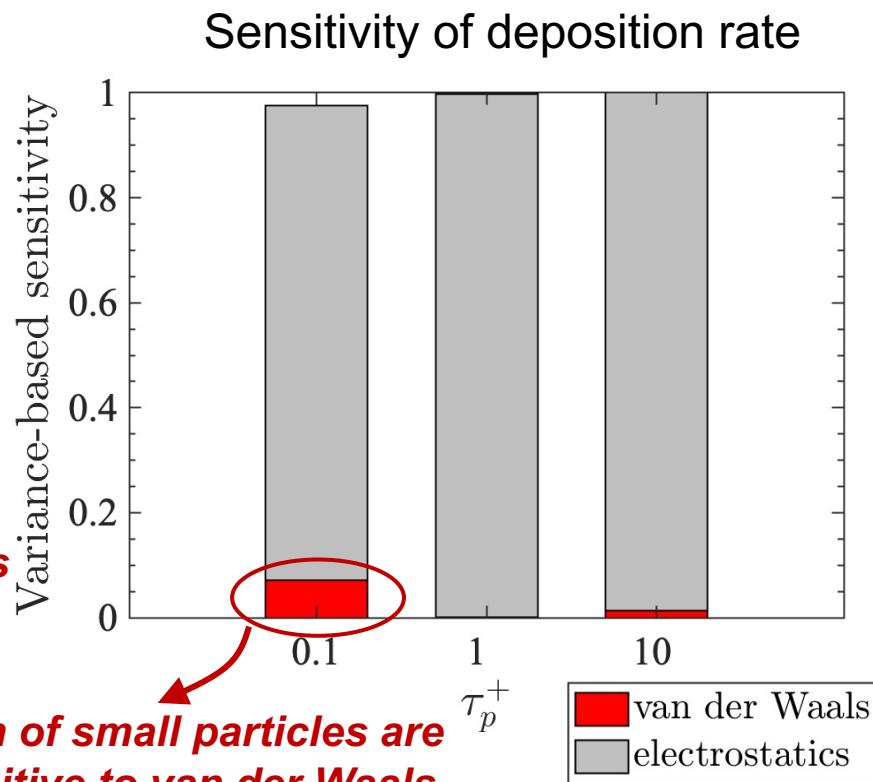
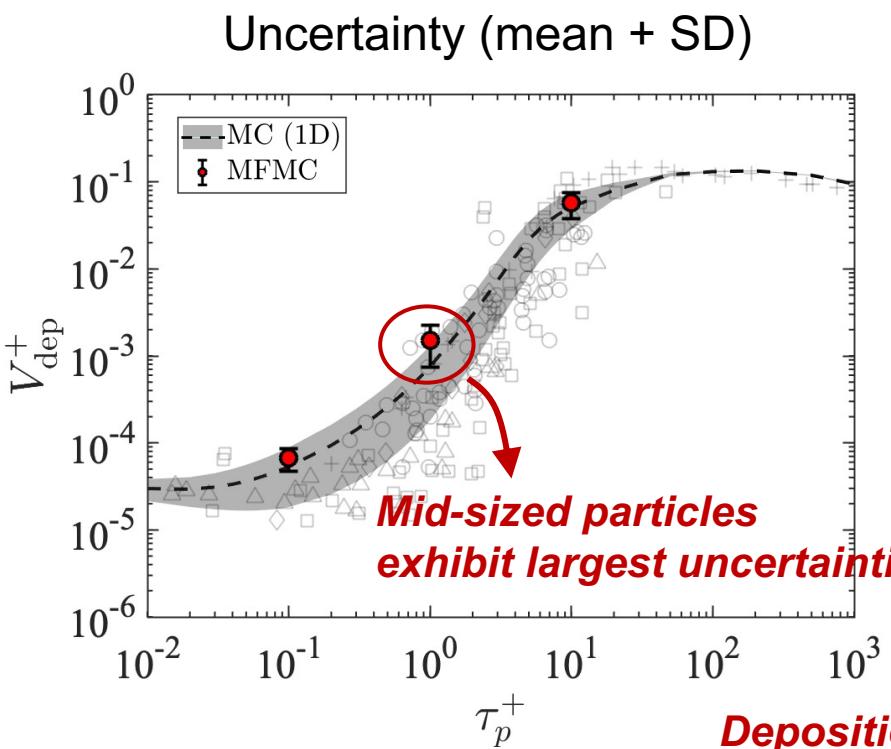
1. Peherstorfer et al. (2018), Siam Review.

# *Solution procedure of MFMC UQ on deposition rates*

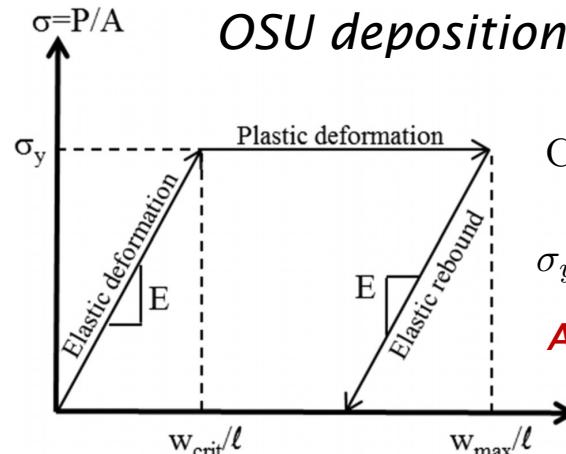
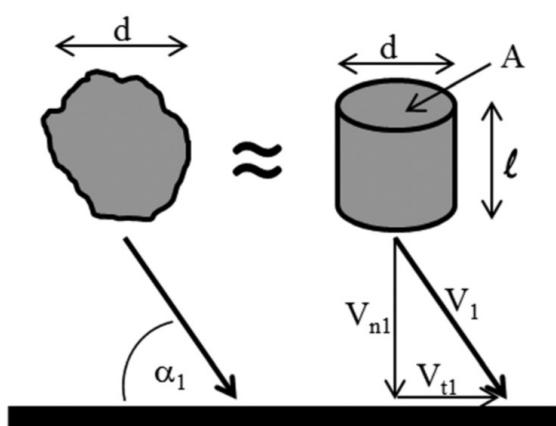


# *Uncertainty and sensitivity of deposition for three particle sizes*

**Mean, standard deviation, and sensitivity of deposition rate are estimated using the multi-fidelity approach with budget  $p=144$  ( $\sim 40,000$  CPU hours)**



# *Effect of cohesion and temperature on particle rebound*



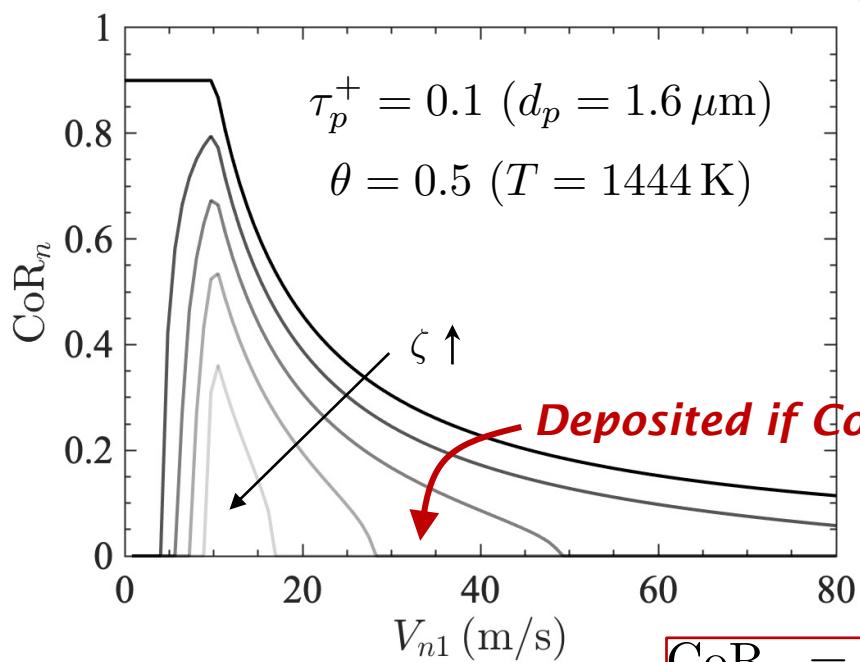
*OSU deposition model (Bons et al 2017):*

$$\text{CoR}_n = \frac{V_{n2}}{V_{n1}} = \sqrt{\frac{\sigma_y^2}{\rho E} - \frac{2A_{\text{cont}}\gamma}{m}} \frac{1}{V_{n1}}$$

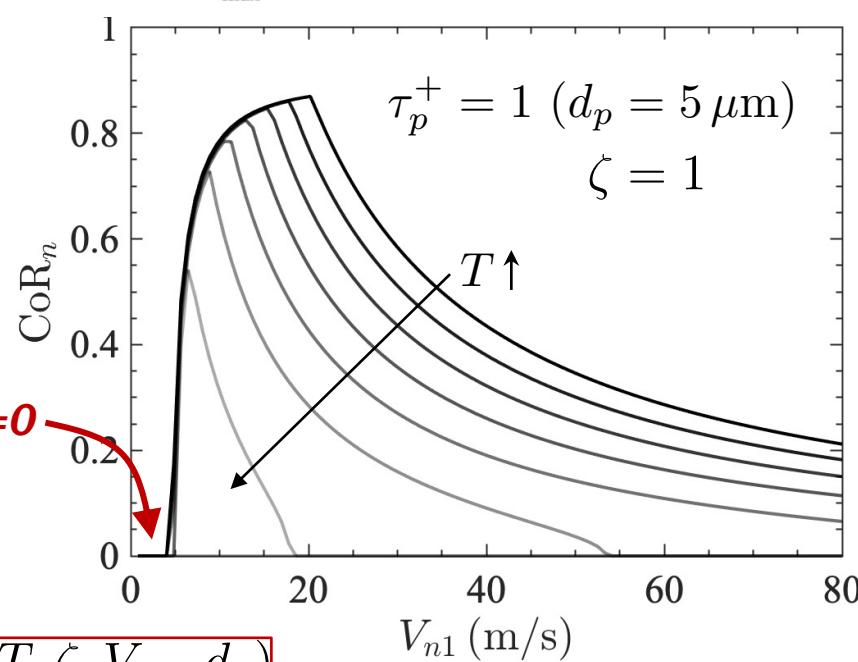
$$\sigma_y(T) = 200 - 0.225(T - 1000) \text{ (MPa)}$$

**Additional input parameter:**

$$\theta = 0.225(T - 1000)/200 \in [0, 1]$$



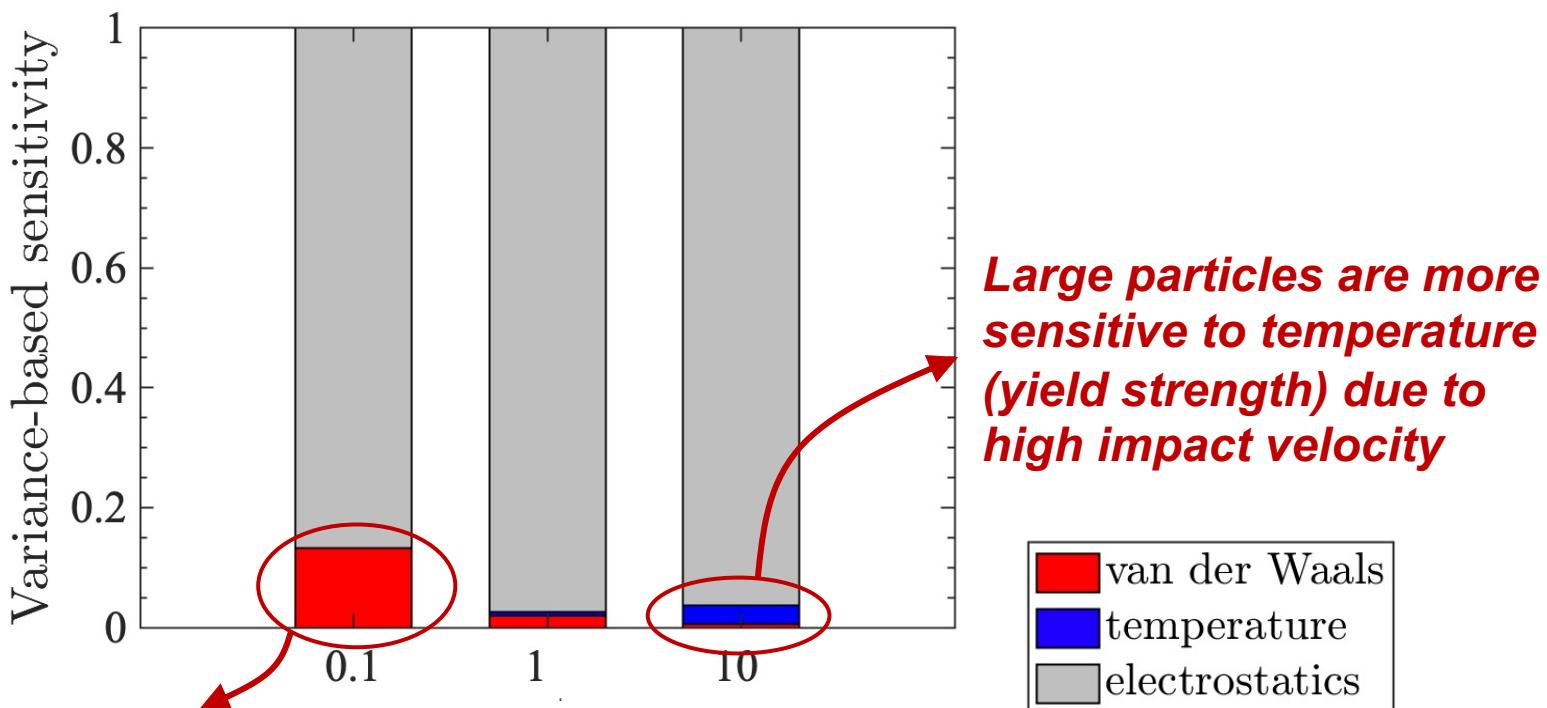
$$\text{CoR}_n = f(T, \zeta, V_{n1}, d_p)$$



## *Sensitivity of Capture Efficiency (CE) on temperature*

- 1D model and DNS are modified to include OSU deposition model
- Capture efficiency is typically measured in experiments:

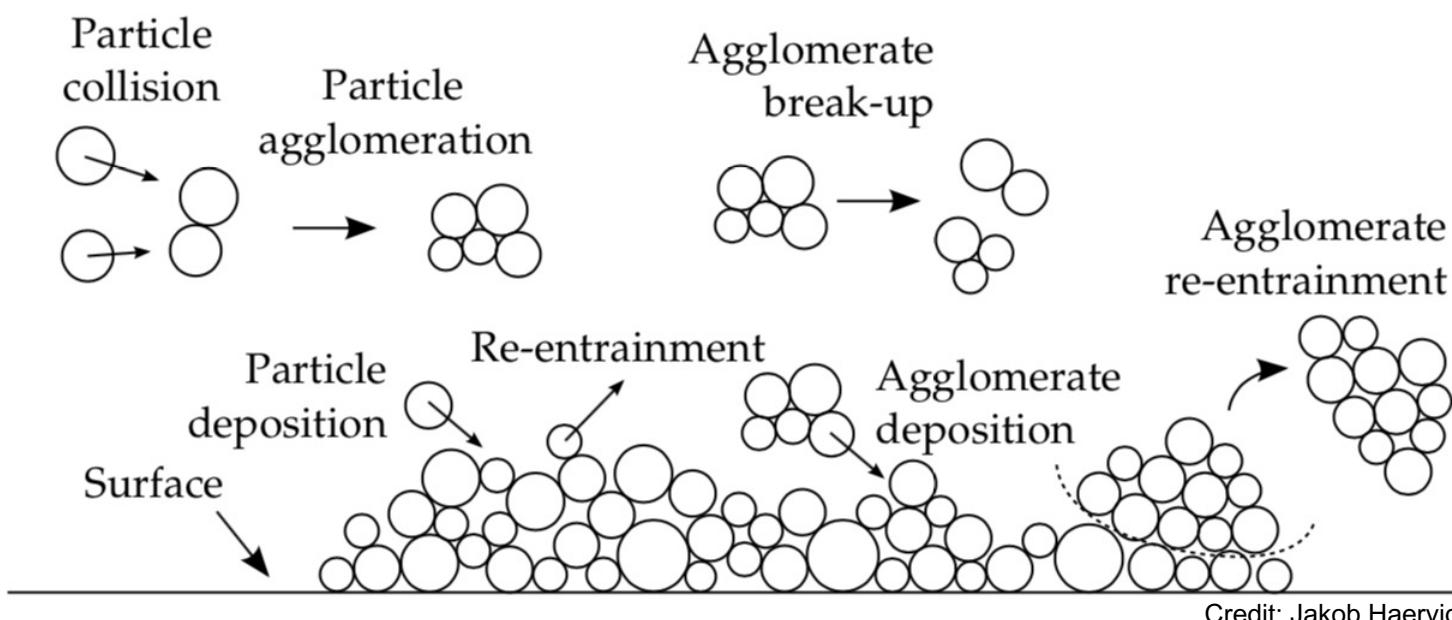
$$CE = \frac{\dot{m}_{\text{dep}}}{\dot{m}_{\text{tot}}} = \frac{4L}{D} \frac{u_*}{U_b} V_{\text{dep}}^+$$



# *Conclusions*

1. A multi-fidelity approach was employed to optimally estimate **mean**, **variance**, and **sensitivity** of the deposition rate.
  - Cheap 1D models were evaluated to reduce the cost while retaining accuracy guarantees of expensive DNS.
2. Deposition was found more sensitive to **electrostatics** than van der Waals across all particle sizes and exhibited largest uncertainty for **mid-sized** particles.
3. All-stick assumption is more valid for **small particles** whose deposition is more sensitive to cohesion and less sensitive to temperature

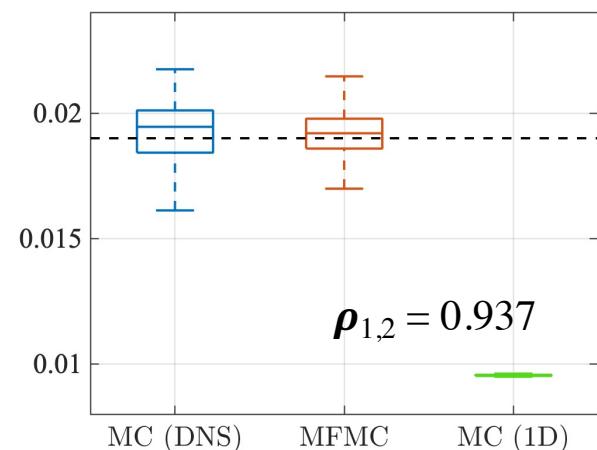
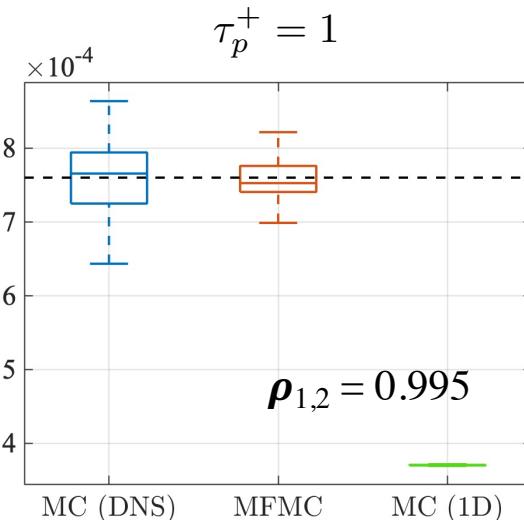
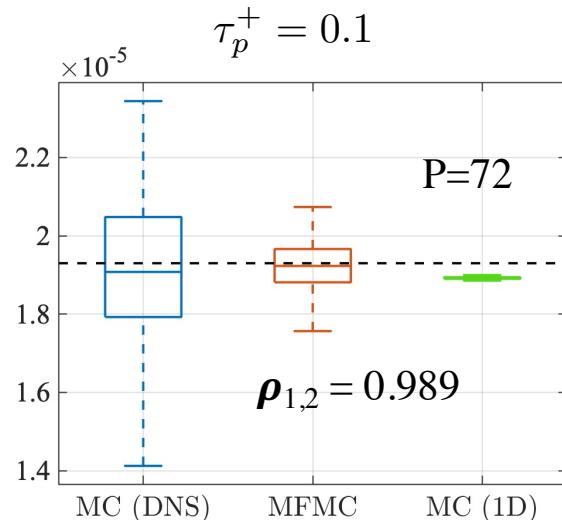
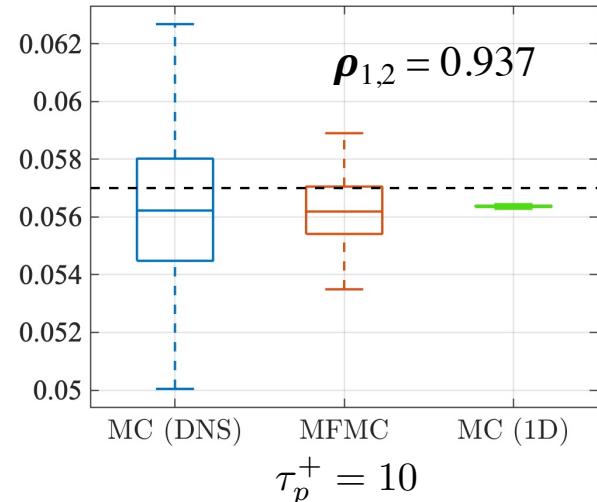
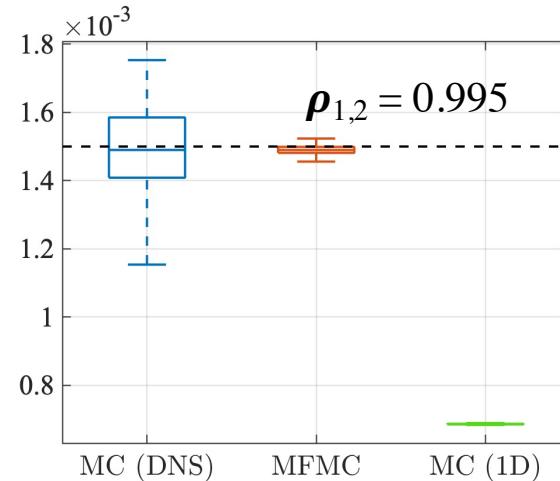
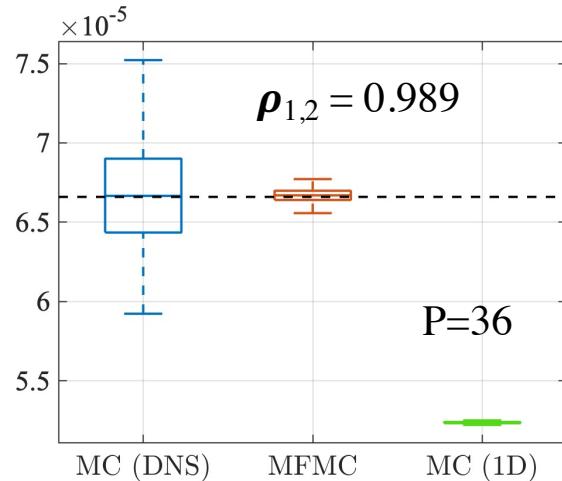
# Questions?



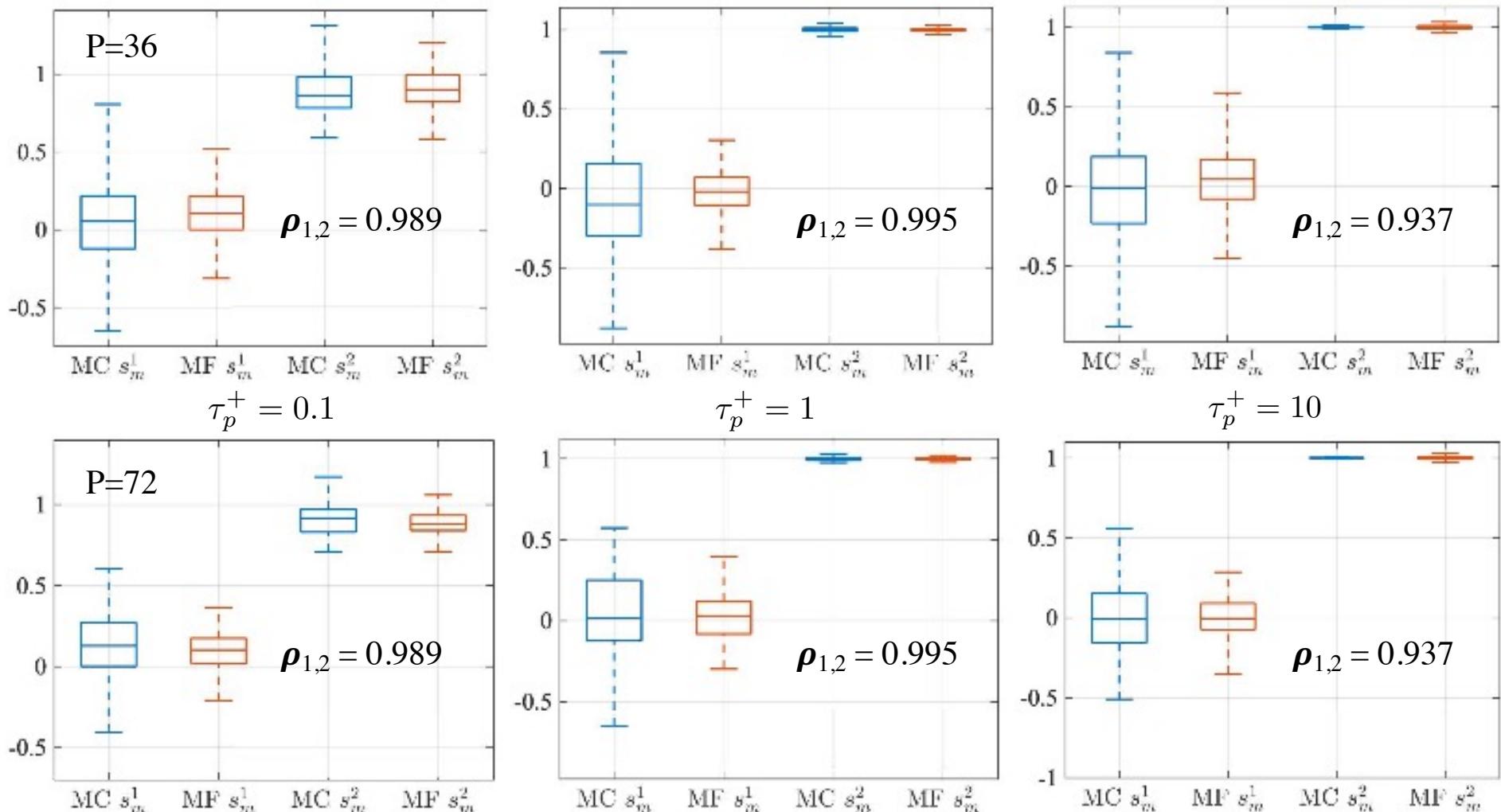
Credit: Jakob Haervig



# *Uncertainties of deposition rate to charge and van der Waals*



# *Sensitivity of deposition rate to charge and van der Waals*



# Multi-fidelity Uncertainty Quantification

- An analytical solution exists for the optimal number of evaluations for each model

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**Algorithm 2.** Multifidelity Monte Carlo.

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- 1: **procedure** MFMC( $f^{(1)}, \dots, f^{(k)}, \bar{\sigma}_1, \dots, \bar{\sigma}_k, \bar{\rho}_{1,1}, \dots, \bar{\rho}_{1,k}, w_1, \dots, w_k, p$ )
- 2:     Ensure  $f^{(1)}, \dots, f^{(k)}$  is the result of mSELECT defined in Algorithm 1
- 3:     Set  $\bar{\rho}_{1,k+1} = 0$  and define vector  $\bar{\mathbf{r}} = [\bar{r}_1, \dots, \bar{r}_k]^T \in \mathbb{R}_+^k$  as

$$\bar{r}_i = \sqrt{\frac{w_1(\bar{\rho}_{1,i}^2 - \bar{\rho}_{1,i+1}^2)}{w_i(1 - \bar{\rho}_{1,2}^2)}}, \quad i = 1, \dots, k$$

- 4:     Select number of model evaluations  $\mathbf{m} \in \mathbb{R}_+^k$  as

$$\mathbf{m} = \left[ \frac{p}{\mathbf{w}^T \bar{\mathbf{r}}}, \bar{r}_2 m_1, \dots, \bar{r}_k m_1 \right]^T \in \mathbb{R}_+^k$$

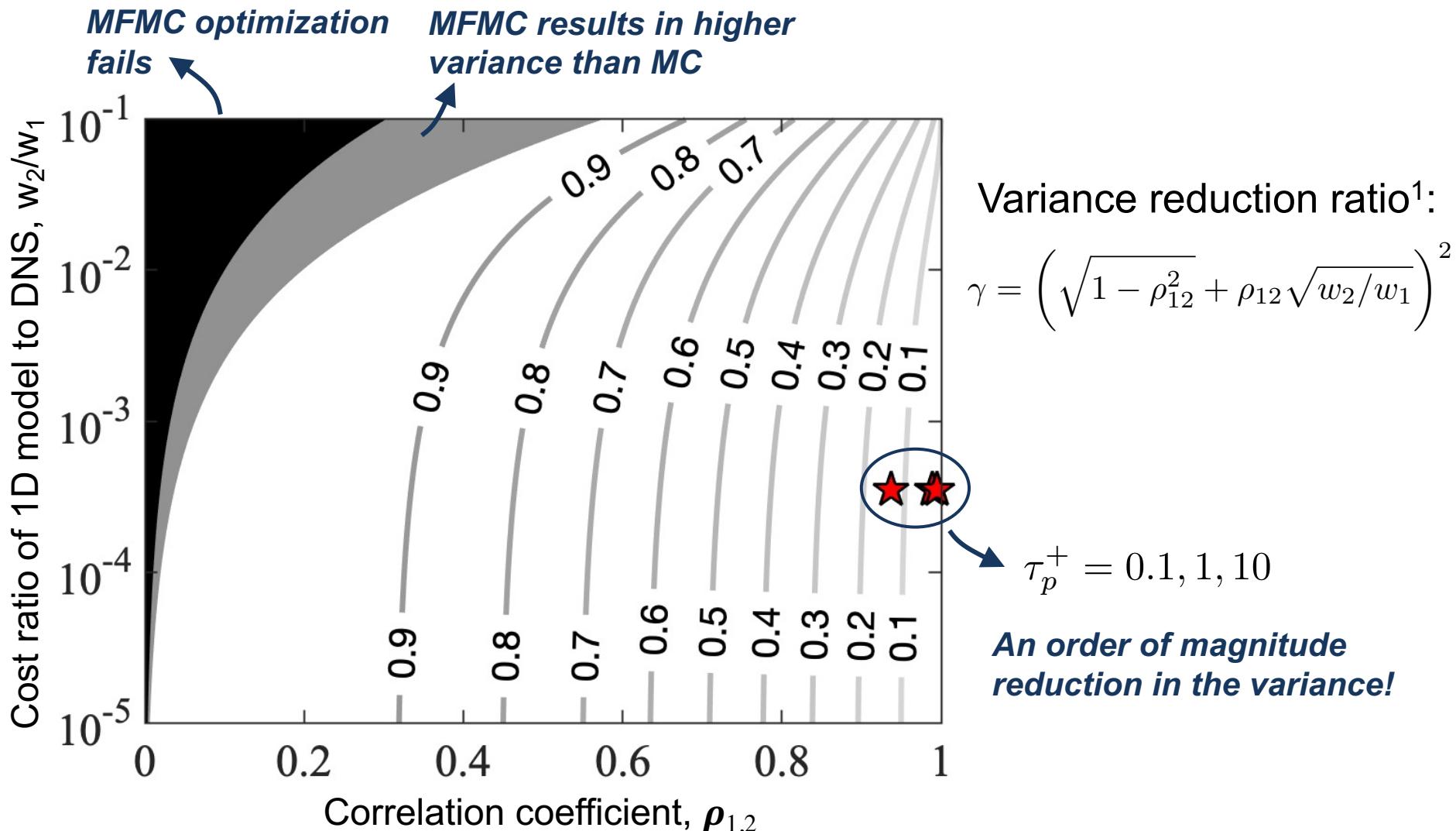
- 5:     Round down components of  $\mathbf{m}$  to obtain integers
- 6:     Set coefficients  $\boldsymbol{\alpha} = [\alpha_1, \dots, \alpha_k]^T \in \mathbb{R}^k$  to

$$\alpha_i = \frac{\bar{\rho}_{1,i} \bar{\sigma}_1}{\bar{\sigma}_i}, \quad i = 1, \dots, k$$

- 7:     Draw  $\mathbf{z}_1, \dots, \mathbf{z}_{m_k} \in \mathcal{D}$  realizations of  $Z$
  - 8:     Evaluate model  $f^{(i)}$  at realizations  $\mathbf{z}_1, \dots, \mathbf{z}_{m_i}$  for  $i = 1, \dots, k$
  - 9:     Compute MFMC estimate  $\hat{s}$  as in (3.2)
  - 10:    **return**  $\hat{s}$
  - 11: **end procedure**
- 

- Advantages:
  - Orders of magnitudes faster than normal UQ
  - Low-fidelity models can take any forms: ROM, coarser mesh, POD/DMD, line fitting etc....
  - Error for each level of model is not required for MFMC UQ

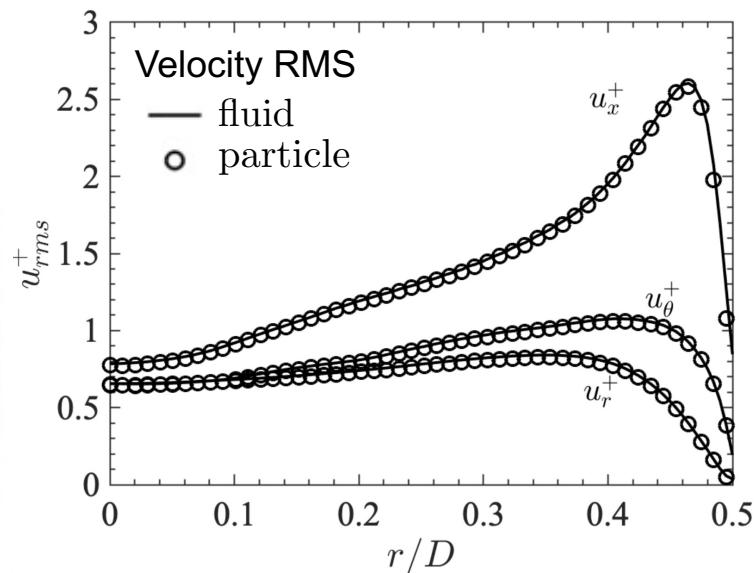
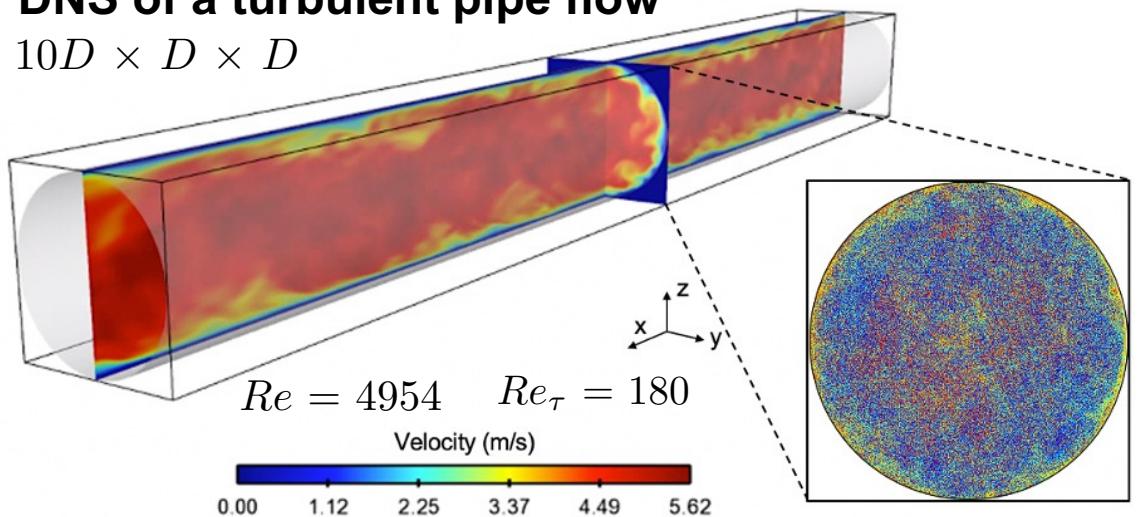
# Reduced variance by leveraging models of different fidelities



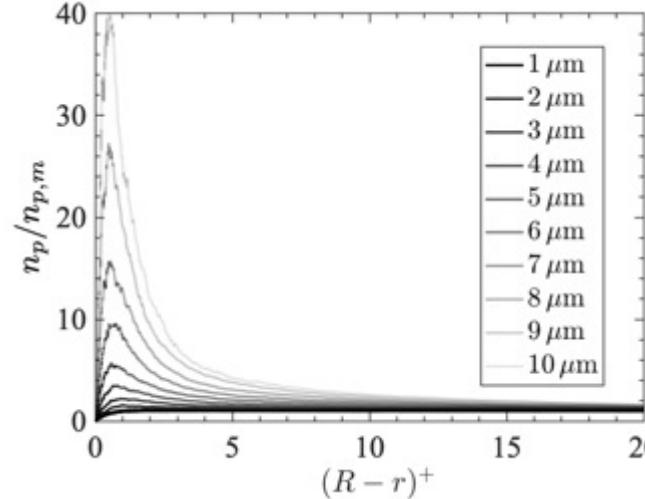
# Charge modifies particle near-wall statistics<sup>1</sup>

## DNS of a turbulent pipe flow

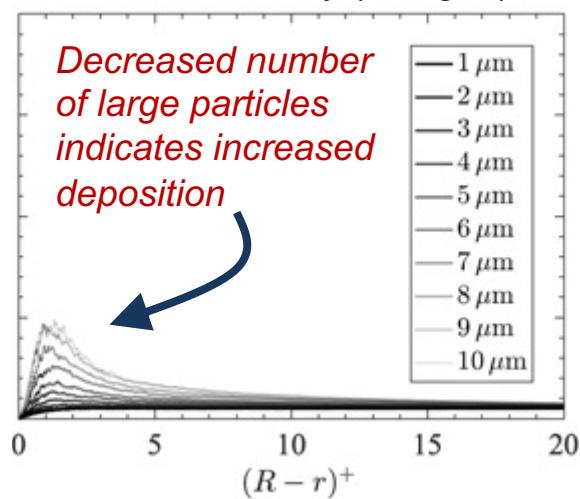
$10D \times D \times D$



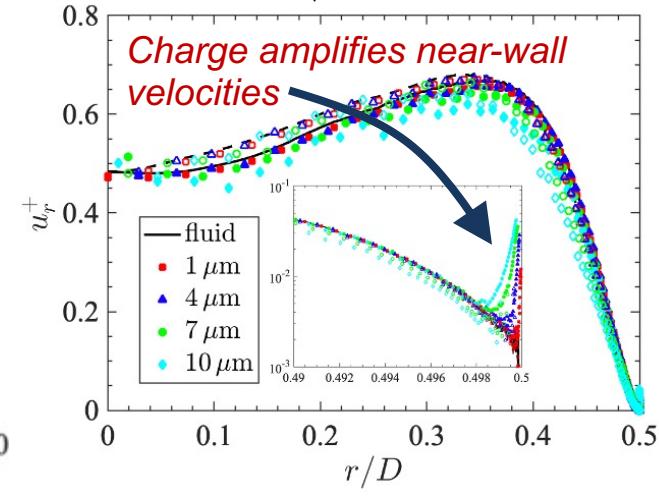
Number density (uncharged)



Number density (charged)

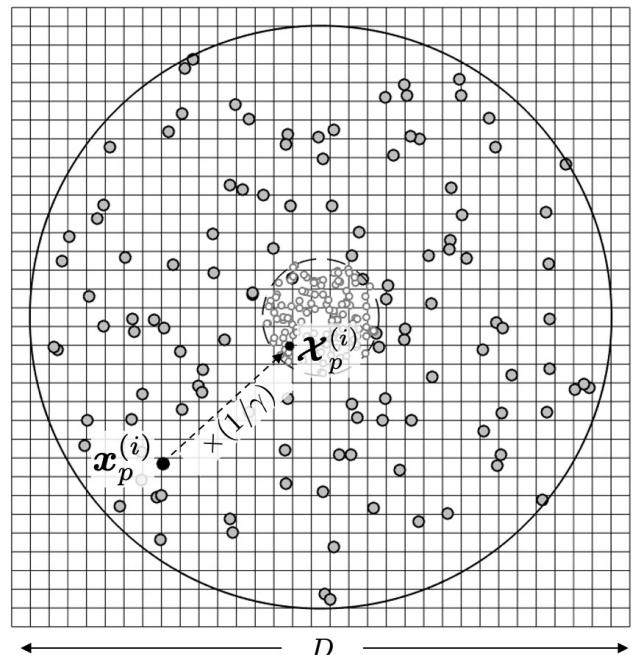


$\xi = 0.1$ , w/ image charging



# Scaled-mapping treatment for non-periodic geometries

- Particles are scaled-mapped inwards by  $\gamma = \mathcal{L}/D$  to remove periodic images<sup>1</sup>:

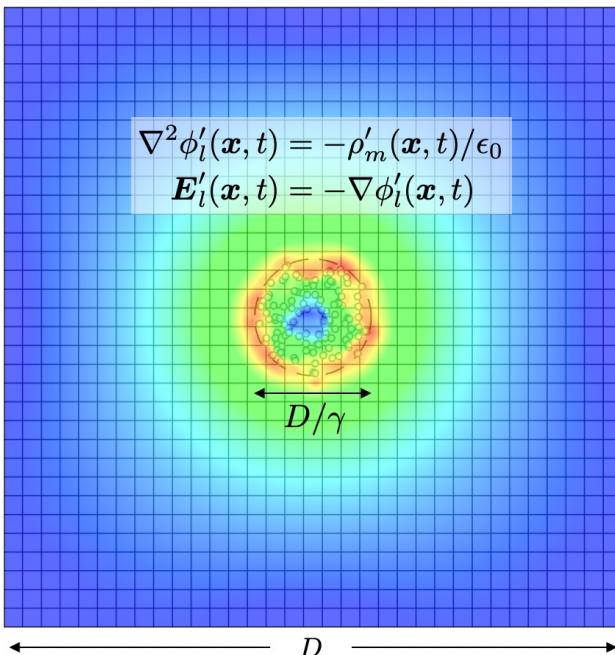


Step 1: particle scaled-mapping

$$* \quad \mathbf{x}_p^{(i)} = \mathbf{x}_p^{(i)} \otimes (1, 1/\gamma, 1/\gamma)$$

$$\rho'_m(\mathbf{x}, t) = \sum_{i=1}^N q_p^{(i)} \mathcal{W} \left( \mathbf{x} - \mathbf{x}_p^{(i)}(t) \right)$$

$$* \quad \rho_m(\mathbf{x}, t) = \rho'_m(\mathbf{x}, t)/\gamma^2$$

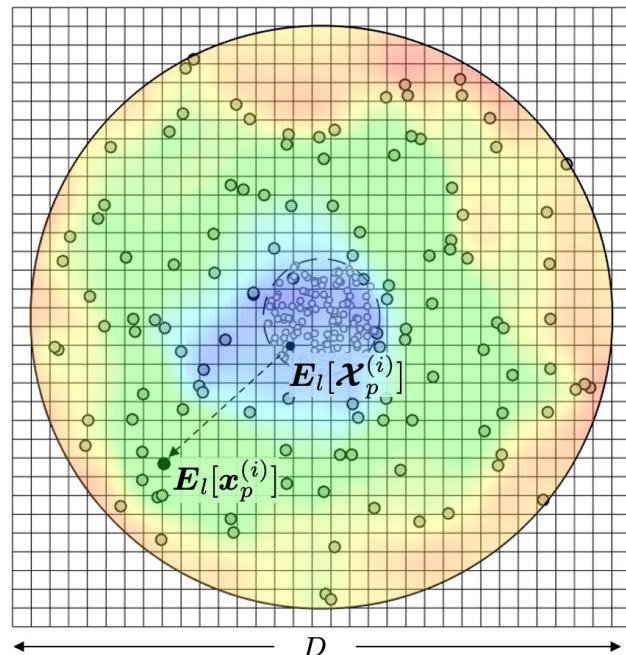


Step 2: solve scaled electrical field

$$\hat{\rho}_l(\mathbf{k}) = \hat{\rho}_m(\mathbf{k}) \hat{G}(\mathbf{k})$$

$$k^2 \hat{\phi}_l(\mathbf{k}) = \frac{\hat{\rho}_l(\mathbf{k})}{\epsilon_0}$$

$$\mathbf{E}'_l(\mathbf{x}, t) = -\nabla \phi_l(\mathbf{x}, t)$$



Step 3: mapping the solutions back

$$* \quad \mathbf{E}_l(\mathbf{x}, t) = \mathbf{E}'_l(\mathbf{x}, t) \otimes (1, 1/\gamma, 1/\gamma)$$

$$* \quad \mathbf{E}_l[\mathbf{x}_p^{(i)}] = \mathbf{E}_l[\mathbf{x}_p^{(i)}]$$

\* indicates additional steps

